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4. Application number(s) or patent number(s): 7,081,203B2 Issued July 25, 2006


If this document is being filed together with a new application, the execution date of the application is: _____

<p>A. Patent Application No.(s)</p>	<p>B. Patent No.(s)</p> <p>7,081,203 B2 Issued: July 25, 2006</p>
Additional numbers attached? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	

<p>5. Name and address of party to whom correspondence concerning document should be mailed:</p> <p>Name: <u>R. Reams Goodloe, Jr.</u></p> <p>Internal Address: _____</p> <p>Street Address: 24722 - 104th Avenue, S.E. Suite 102</p> <p>City: KENT State WA Zip: 98030-5322</p>	<p>6. Total number of applications and patents involved:</p> <p style="text-align: center;">1</p>
<p>Matter No.: <u>VD0-3030-0</u></p>	<p>7. Total fee (37 CFR 3.41)\$ <u>40.00</u></p> <p><input type="checkbox"/> Enclosed</p> <p><input checked="" type="checkbox"/> Authorized to be charged to deposit account</p>
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<u>R. Reams Goodloe, Jr. Reg. #32,466</u> Name of Person Signing	 Signature	<u>October 17, 2006</u> Date
Total number of pages including cover sheet, attachments, and document: <u>30</u>		

Mail documents to be recorded with required cover sheet information to: Commissioner for Patents, Mail Stop Assignment, P.O. Box 1450, ALEXANDRIA, VA 22313-1450. (via Facsimile: Assignments Division, Facsimile No. 571-273-0140 ON 10/17/2006)

ASSIGNMENT OF INVENTION
Attorney Docket No.: VD0-3030-U

For: U.S. and/or Foreign Rights
 For: U.S. Application or
 U.S. Provisional Application
 For: U.S. Patent
 For: PCT Application
 By: Inventor(s) or Present Owner

ASSIGNMENT OF INVENTION

In accord with existing contractual agreements between the ASSIGNOR and the ASSIGNEE, and in consideration of the payment by ASSIGNEE to ASSIGNOR of the sum of TEN DOLLARS (\$10.00), the receipt of which is hereby acknowledged, and for other good and valuable consideration, effective as of the 16th day of March, 2004,

ASSIGNOR:

Inventor(s) or person(s) or
entity(ies) who own the invention

GLENN HELM

type or print name of ASSIGNOR

25448 Port Gamble Road, N.E.,

Poulsbo, Washington 98370
Address

U.S.
Nationality

(if assignment is by person or entity to whom invention was previously assigned and this was recorded in PTO, add the following):

Recorded on _____ Reel _____ Frame: _____

HEREBY SELLS, ASSIGNS AND TRANSFERS TO

ASSIGNEE:

GLENDON BIOFILTER

TECHNOLOGIES, INC.

type or print name of ASSIGNEE

3412 Northwood Drive

Oceanside, California, 92054
Address

a Washington corporation
Nationality

and the successors, assigns and legal representatives of the
ASSIGNEE

(complete one of the following)

- the assignor's entire right, title and interest
 an undivided _____ percent (___%) interest for the
 United States and its territorial possessions

PATENT

ORIGINAL REEL: 018398 FRAME: 0881

ASSIGNMENT OF INVENTION
Attorney Docket No.: VD0-3030-U

(check the following box, if foreign rights are also to be assigned)

- and in all foreign countries, including all rights to claim priority,

in and to any and all improvements which are disclosed in the invention entitled:

COMPACT SURFACE MOUNTED ON-SITE WASTEWATER TREATMENT UNIT

Name of Inventor(s) GLENN HELM

(check and complete (a), (b), (c), (d), (e), (f) or (g))

and which is found in

- (a) U.S. patent application executed on even date herewith;
- (b) U.S. provisional patent application, Serial No. 60/553,819, filed March 16, 2004;
- (c) U.S. patent application, Serial No. 10/839,974 filed May 6, 2004;
- (d) U.S. Patent Application Publication No. US2005/0205491A1 published September 22, 2005;
- (e) U.S. PATENT NO. 7,081,203 B2 ISSUED JULY 25, 2006, a copy of which is attached hereto as Exhibit I;
- (f) To comply with 37 C.F.R. § 3.21 for recordal of this assignment, I, an ASSIGNOR signing below, hereby authorize and request my attorney to insert below the filing date and application number when they become known.
- (g) International application no. PCT/US _____

(also check (f), if foreign application(s) is also being assigned)

- (h) and any legal equivalent thereof in a foreign country, including but not limited to CA patent application no. 2,506,865, filed May 5, 2005,

and, in and to, all Letters Patent obtained for said invention by the above applications or any continuation, continuation-in-part, division, renewal, or substitute thereof, and as to letters patent on any reissue or re-examination thereof.

ASSIGNOR hereby warrants, represents, and covenants that no assignment, sale, agreement or encumbrance has been or will be made or entered into which would conflict with this Assignment.

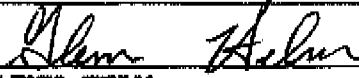
ASSIGNOR further covenants that ASSIGNOR will, upon ASSIGNEE'S request, be provided promptly with all pertinent facts and documents relating to said invention and said Letters Patent and legal equivalents as may be known and

ASSIGNMENT OF INVENTION
Attorney Docket No.: VD0-3030-U

accessible to ASSIGNOR and will testify to the same in any interference, litigation or other proceeding related thereto, and will promptly execute and deliver to ASSIGNEE or its legal representatives any and all papers, instruments, or affidavits required to apply for, obtain, maintain, issue and enforce said application, said invention, and said Letters Patent, and said equivalents thereof which may be necessary to desirable to carry out the purposes hereof and thereof.

IN WITNESS WHEREOF, I have hereunto set my hand and seal on the date shown below.

WARNING: The date of signing must be the same as the date of execution of the application, if item (a) was checked above.

Date: 26 SEPT 2006	 _____ GLENN HELM
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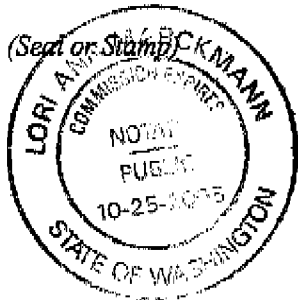
NOTE: No witnessing, notarization or legalization is necessary. If the assignment is notarized or legalized, then it will only be prima facie evidence of execution. 35 U.S.C. § 261. Use next page if notarization is desired.

Notarization or Legalization Page added.

STATE OF WASHINGTON)
COUNTY OF Kitsap) ss.

On this 21st day of September, 2006, before me personally appeared GLENN HELM, personally known to me (or proved to me on the basis of satisfactory evidence) to be the person who is described in and who executed the above instrument, and acknowledged to me that he executed it.

WITNESS my hand and official seal:



Lori Ann Marckmann
Notary Signature
Lori Ann Marckmann
Print Name

Notary Public in and for the State of Washington,
residing at Poulsbo
My appointment expires 10-25-08

ACKNOWLEDGED AND ACCEPTED:

GLENDON BIOFILTER
TECHNOLOGIES, INC.
A Washington Corporation

Thomas Teal
By: THOMAS TEAL
Its: President

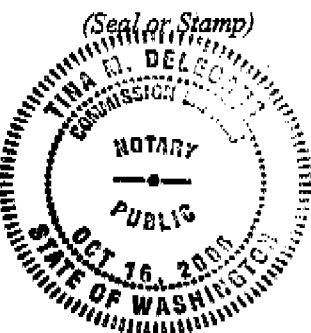
Date: 10-12-06

STATE OF Washington)
COUNTY OF Kent) ss.

Date: 12 October, 2006.

I certify that I know or have satisfactory evidence that THOMAS TEAL is the person who appeared before me, and said person acknowledged that he signed this instrument, on oath stated that he was authorized to execute the instrument and acknowledged it as the President of GLENDON BIOFILTER TECHNOLOGIES, INC., to be the free and voluntary act of such party, for the uses and purposes mentioned in the instrument.

WITNESS my hand and official seal:



Tina M. DeLegans
Notary Signature
Tina M. DeLegans
Print Name

Notary Public in and for the State of WA
residing at Kent, WA
My appointment expires 16 October 2006



US007081203B2

(12) **United States Patent**
Helm

(10) **Patent No.:** US 7,081,203 B2
(45) **Date of Patent:** Jul. 25, 2006

(54) **COMPACT SURFACE MOUNTED ON-SITE WASTEWATER TREATMENT UNIT**

(76) **Inventor:** Glenn Helm, 25448 Port Gamble Rd. NE, Poulsbo, WA (US) 98370

(*) **Notice:** Subject to any disclaimer, the term of this patent is extended or adjusted under 35 U.S.C. 154(b) by 54 days.

(21) **Appl. No.:** 10/839,974

(22) **Filed:** May 6, 2004

(65) **Prior Publication Data**
US 2005/0205491 A1 Sep. 22, 2005

Related U.S. Application Data
(60) Provisional application No. 60/553,819, filed on Mar. 16, 2004.

(51) **Int. Cl.** (2006.01)
C02F 3/06
(52) **U.S. Cl.** 210/617; 210/747; 210/150; 210/151; 210/170; 210/532.2

(58) **Field of Classification Search** 210/617, 210/797, 150, 151, 170, 259, 299, 265, 266, 210/532.2
See application file for complete search history.

(56) **References Cited**

U.S. PATENT DOCUMENTS

212,023 A	2/1879	Maeurer	
690,333 A	12/1901	Wanner	
699,345 A	5/1902	Provost, Jr.	
800,187 A *	9/1905	Venable	210/150
956,665 A *	5/1910	Ashley	210/150
1,738,521 A	12/1929	Bombhoff	
1,950,841 A *	3/1934	Crawford	210/150
2,590,964 A	4/1952	Halverson	
3,123,556 A	3/1964	Gilbert	
3,126,333 A	3/1964	Williams	
3,215,274 A	11/1965	Schreiber	

3,219,577 A	11/1965	Powers, III	
3,238,124 A	3/1966	Burton	
3,407,935 A	10/1968	Burton	
3,543,937 A	12/1970	Choun	
3,617,541 A	11/1971	Pan	
3,770,623 A *	11/1973	Seidel	210/170
3,774,768 A	11/1973	Turner	
3,882,027 A *	5/1975	Lunt	210/150
3,925,206 A *	12/1975	Dea	210/170
3,933,629 A	1/1976	Smith	
3,950,252 A	4/1976	Jordan et al.	
3,957,634 A	5/1976	Orensten et al.	

(Continued)

FOREIGN PATENT DOCUMENTS

CA 2065350 3/1991

(Continued)

Primary Examiner—Christopher Upton
(74) *Attorney, Agent, or Firm*—R. Reams Goodloe, Jr.

(57) **ABSTRACT**

A compact, ground surface mounted wastewater treatment unit module. The module is surface mounted on a selected substrate such as a scarified native soil. A watertight receiving basin is located on the substrate. The basin is at least partially filled with a lower layer of packing media, suitable for support of biological growth, and then with at least a first and a final layer of a porous granular media. A standpipe introduces wastewater to be treated, and such wastewater is distributed to the packing at the lower reaches of the basin. The wastewater flows up through the packing, and into the first layer of a porous granular media, and thence upwardly and outwardly via capillary action and molecular attraction, and ultimately through the final porous granular media. Treated wastewater is either collected or absorbed in an absorption foot interface between the final medium and the native earth below.

67 Claims, 11 Drawing Sheets

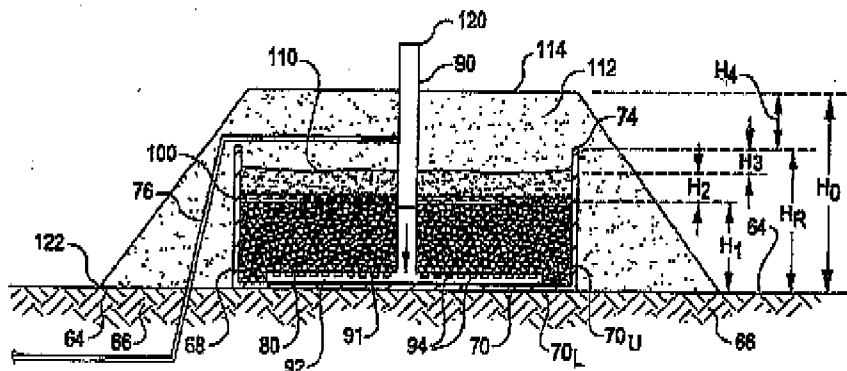


EXHIBIT I

US 7,081,203 B2

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U.S. PATENT DOCUMENTS

4,162,976 A	7/1979	Monson		5,893,975 A *	4/1999	Eifert	210/617
4,169,050 A	9/1979	Scriffling et al.		5,958,239 A	9/1999	Sing	
4,211,653 A	7/1980	Jordan		5,980,739 A	11/1999	Jowett et al.	
4,218,318 A *	8/1980	Niimi et al.	210/150	5,989,416 A *	11/1999	Gorton	210/151
4,251,359 A	2/1981	Colwell et al.		6,153,094 A	11/2000	Jowett et al.	
4,293,421 A	10/1981	Green		6,210,578 B1	4/2001	Sagastume et al.	
4,311,593 A	1/1982	Benjes et al.		6,264,838 B1	7/2001	Nivens, Jr.	
4,411,780 A	10/1983	Suzuki et al.		6,283,309 B1	9/2001	Koers	
4,422,930 A	12/1983	Hatanaka		6,319,403 B1	11/2001	Meyers	
4,627,917 A	12/1986	Morper		6,319,405 B1	11/2001	Roy et al.	
4,664,803 A	5/1987	Fuchs et al.		6,334,938 B1	1/2002	Ruskin	
4,670,148 A	6/1987	Schneider		6,372,137 B1	4/2002	Bounds	
4,800,021 A	1/1989	Desbos		6,428,239 B1*	8/2002	Davis	210/532.2
4,997,568 A	3/1991	Vanderveelde et al.		6,428,691 B1 *	8/2002	Wofford	210/151
5,043,061 A	8/1991	Inagaki		6,464,865 B1 *	10/2002	Tipton et al.	210/532.2
5,217,616 A	6/1993	Sanyal et al.		6,531,062 B1	3/2003	Whitehill	
5,281,332 A	1/1994	Vanderveelde et al.		6,540,910 B1	4/2003	Schwarzenegger et al.	
5,338,131 A	8/1994	Bestmann		6,569,321 B1	5/2003	Coffman	
5,352,357 A	10/1994	Perry					
5,397,474 A	3/1995	Henry					
5,478,464 A	12/1995	Cyr					
5,480,561 A	1/1996	Ball et al.					
5,503,738 A	4/1996	DeFilippi et al.					
5,543,039 A *	8/1996	Odegaard	210/150				
5,578,202 A	11/1996	Hirane					
5,632,896 A	5/1997	Vanderveelde et al.					
5,707,513 A	1/1998	Jowett et al.					
5,766,454 A	6/1998	Cox et al.					
5,766,475 A	6/1998	Mayer et al.					

FOREIGN PATENT DOCUMENTS

CA	2073969	6/2001
GB	18216	10/1893
JP	49-19788	5/1974
JP	56-31152	7/1981
JP	57-148498	9/1982
JP	3068645	5/2000
WO	WO 91/03429	3/1991
WO	WO 91/10624	7/1991

* cited by examiner

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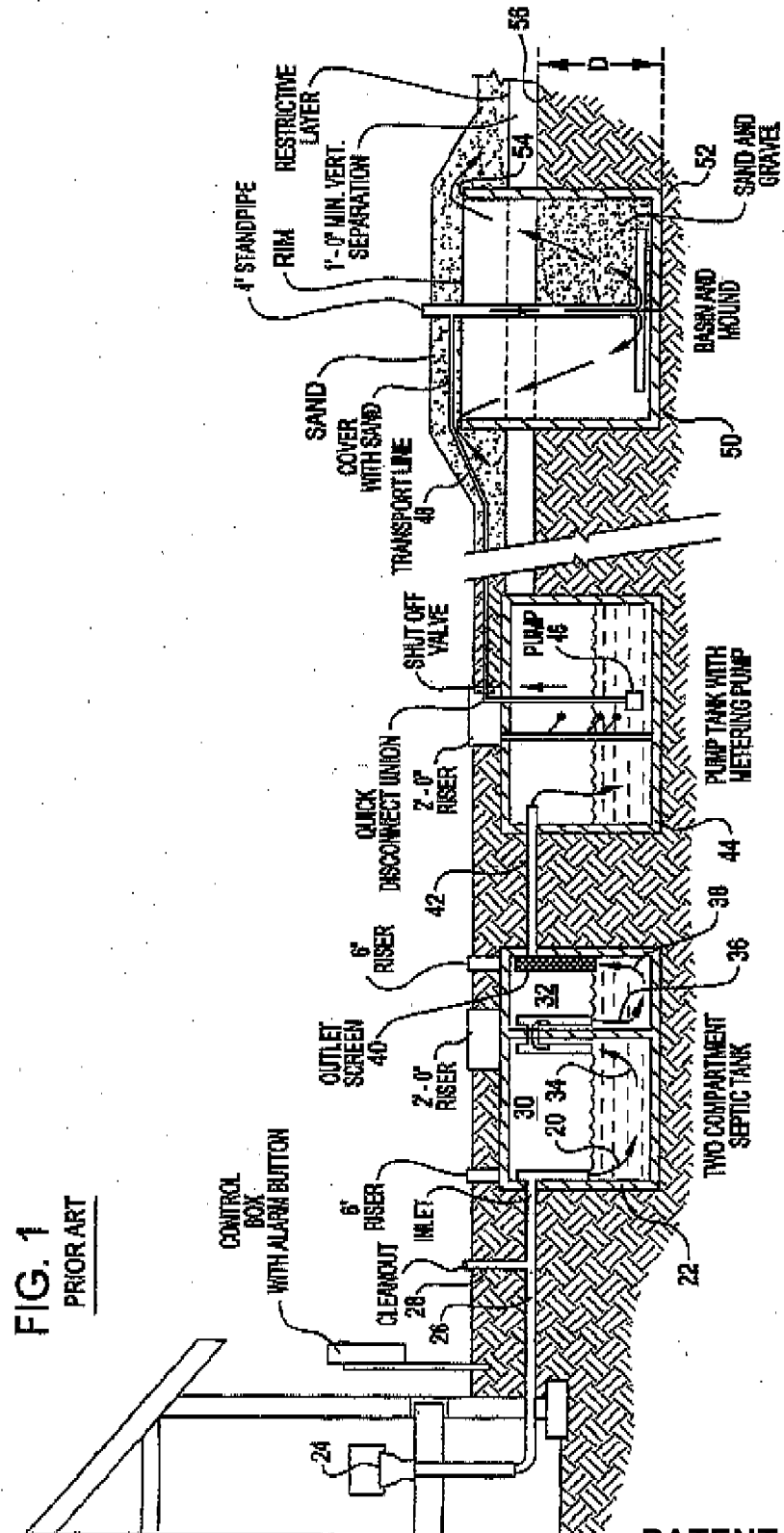


FIG. 1
PRIOR ART

PATENT

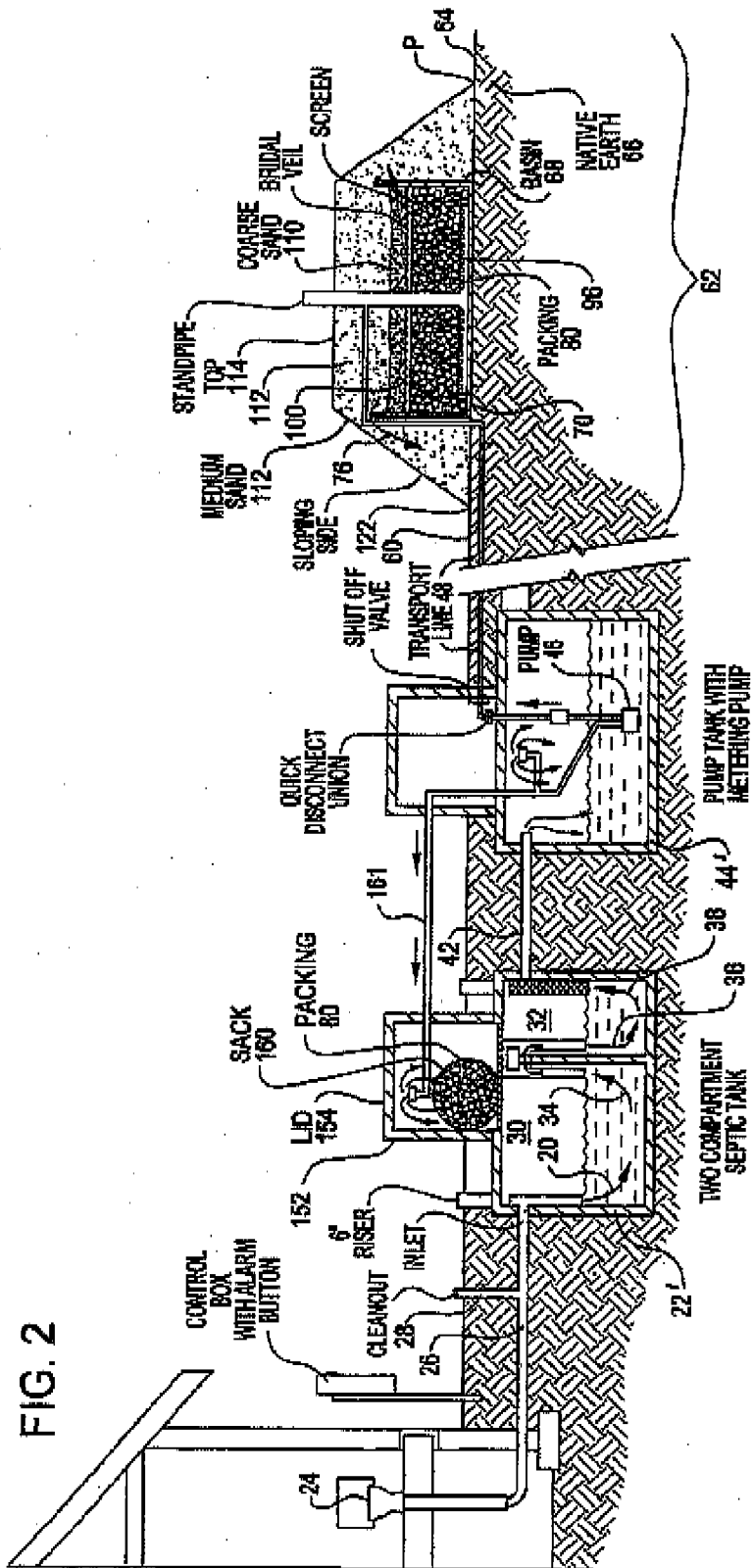
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PATENT

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FIG. 3

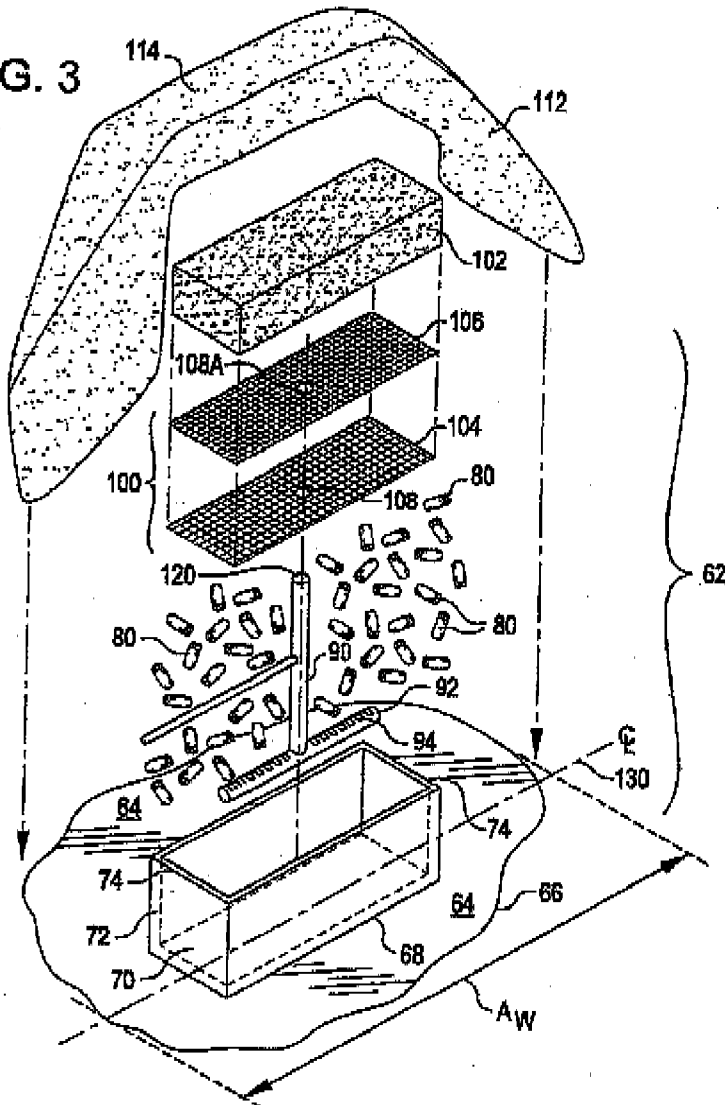
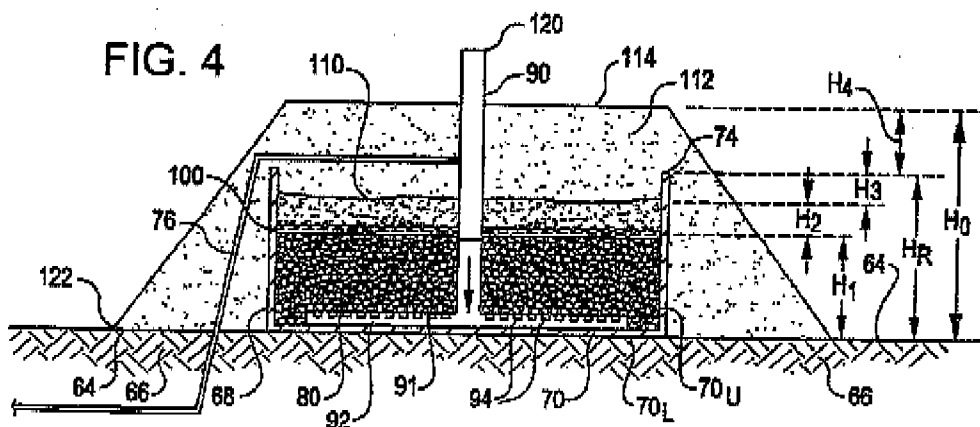


FIG. 4



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FIG. 5

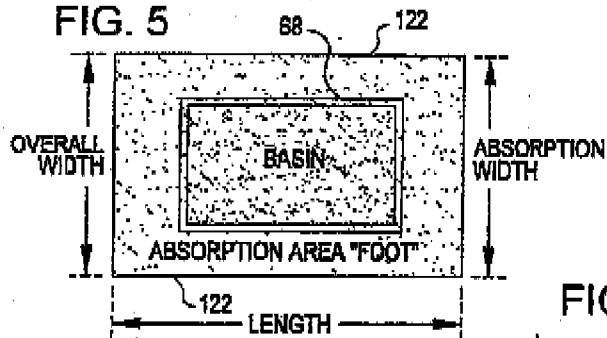


FIG. 6

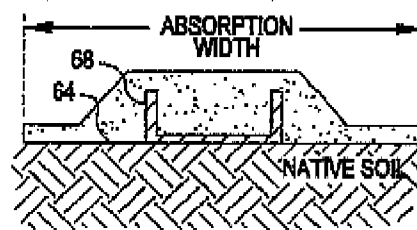


FIG. 7

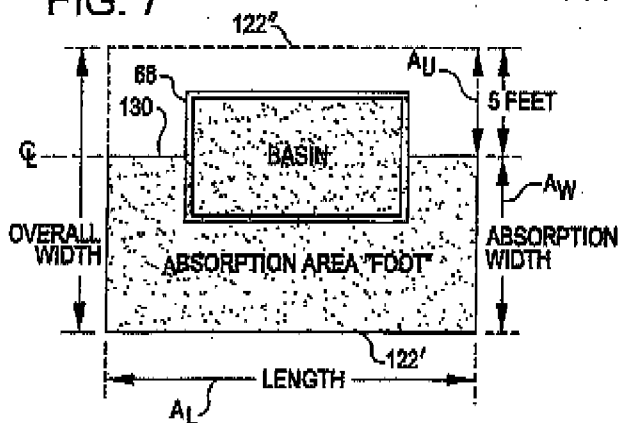


FIG. 9

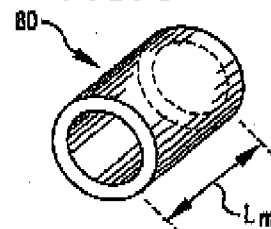


FIG. 8

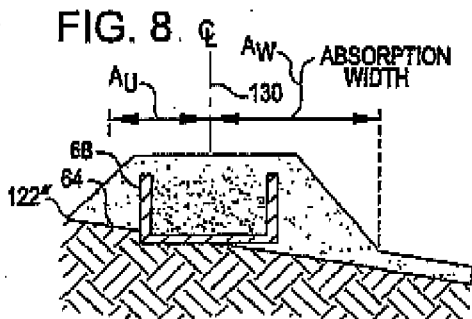
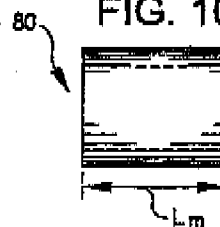


FIG. 10



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FIG. 11

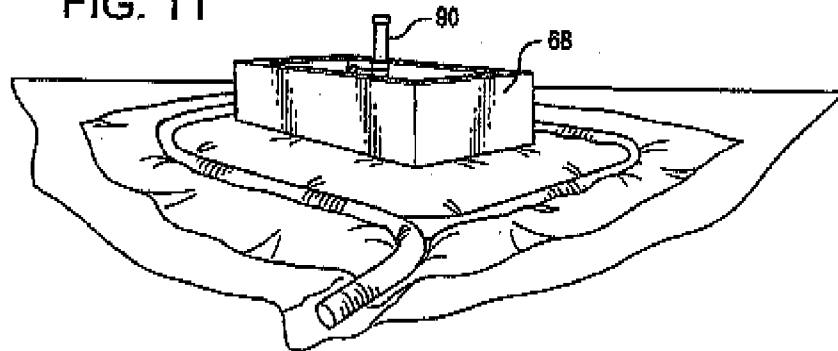


FIG. 12

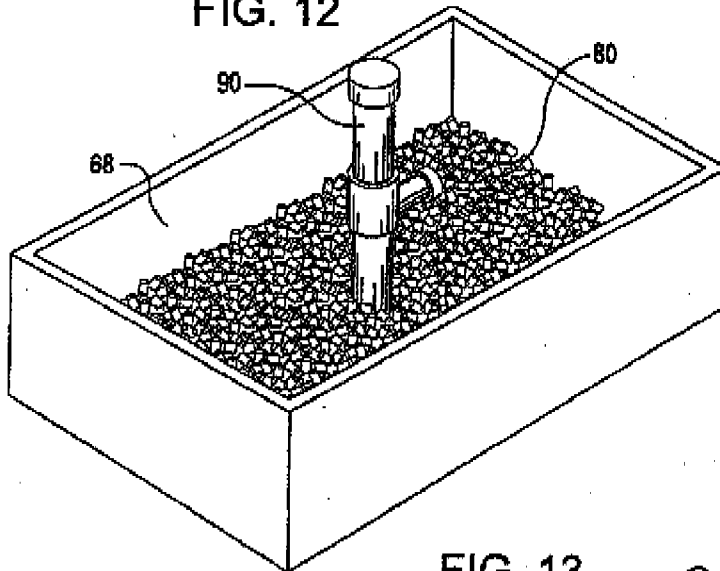
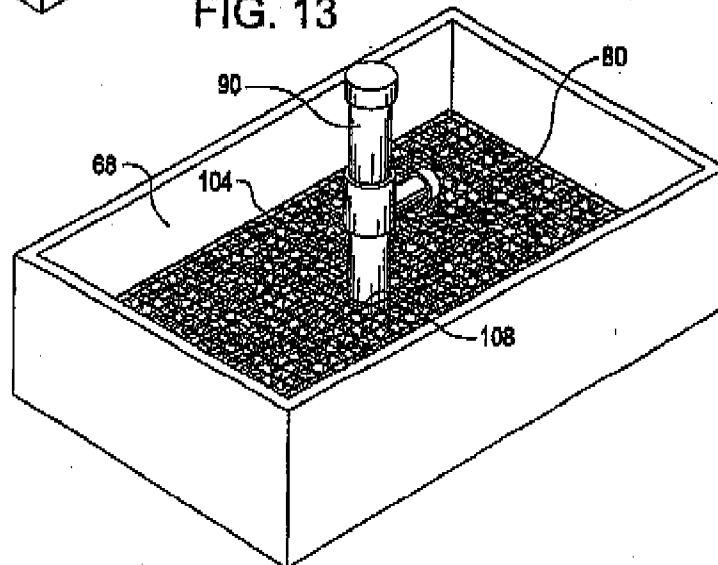


FIG. 13



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FIG. 14

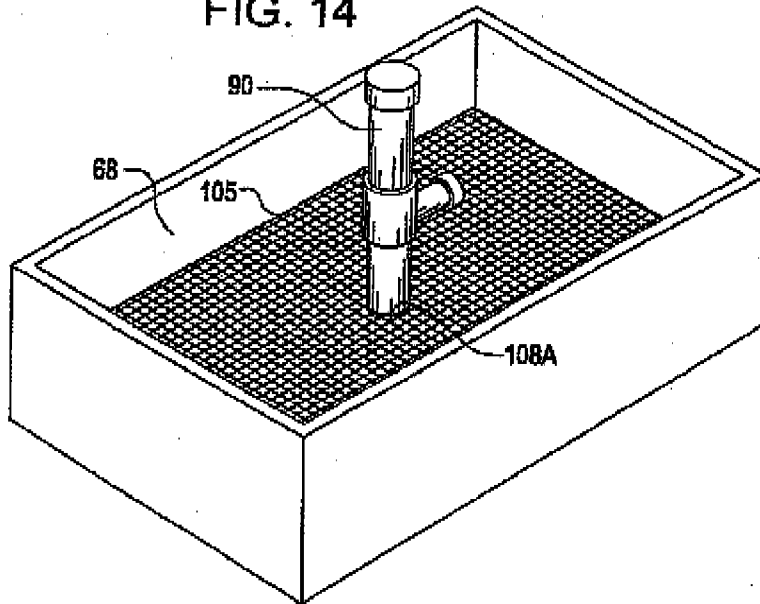
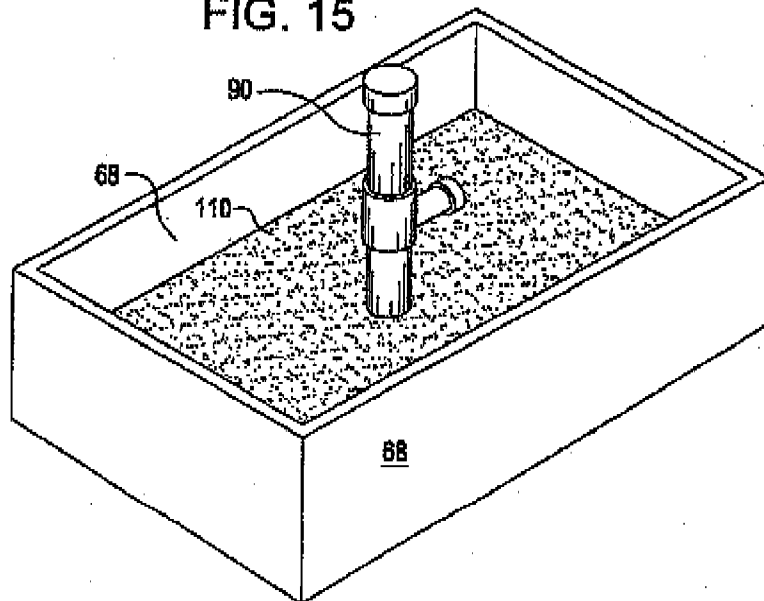


FIG. 15



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FIG. 16

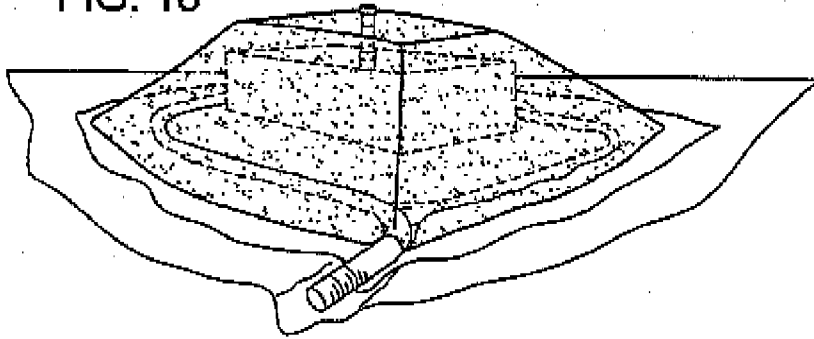


FIG. 20

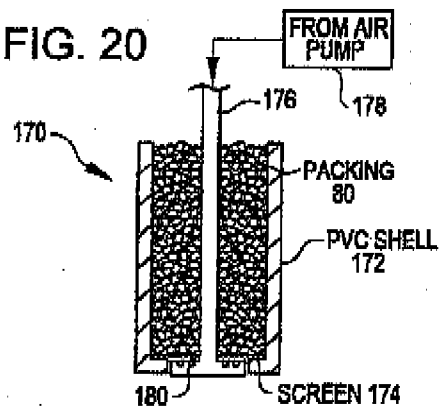
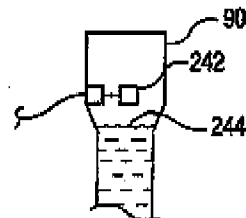


FIG. 23



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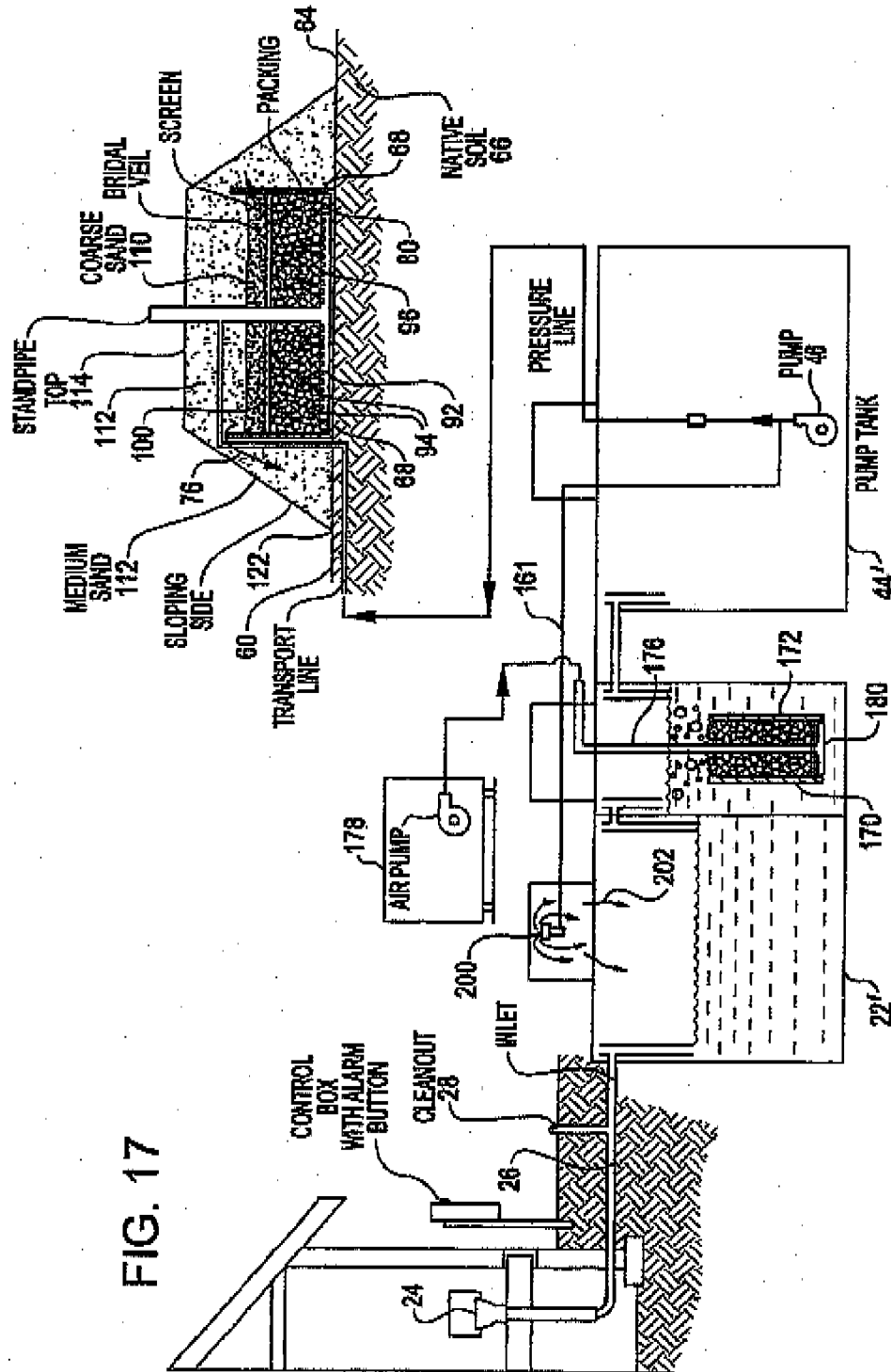


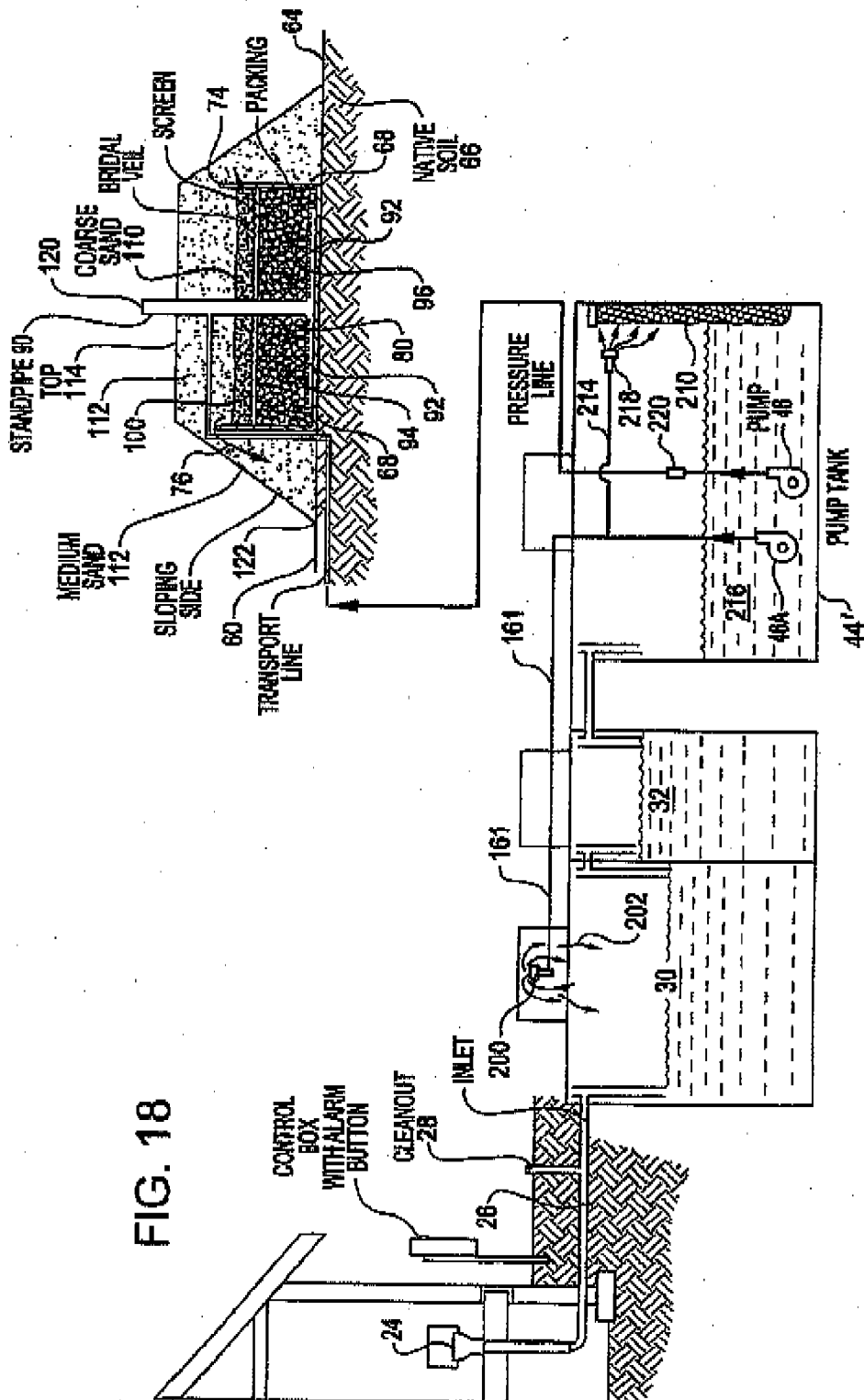
FIG. 17

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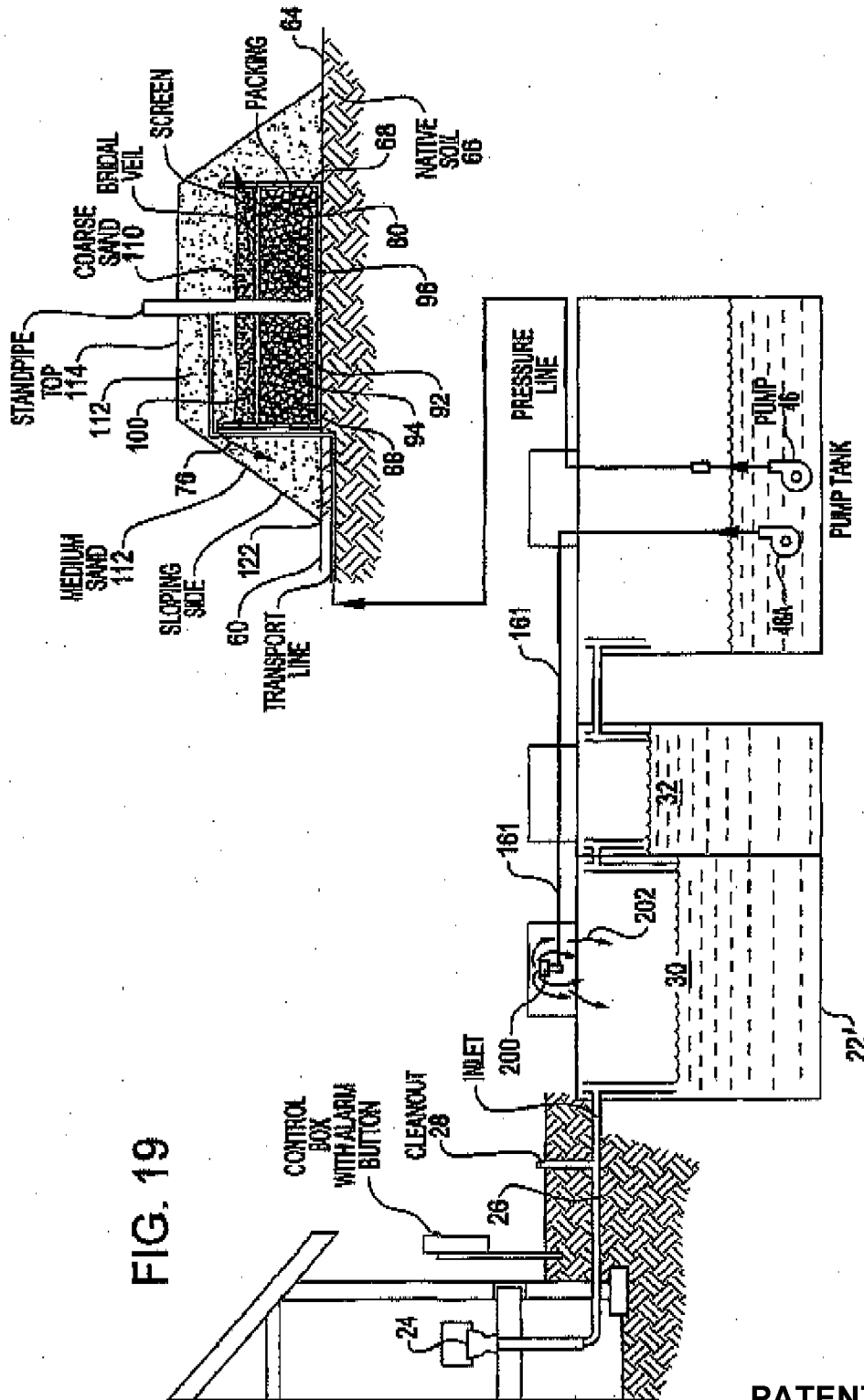


FIG. 19

PATENT

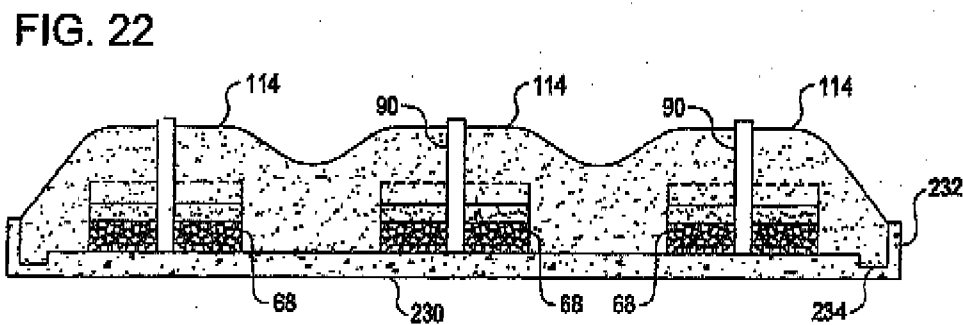
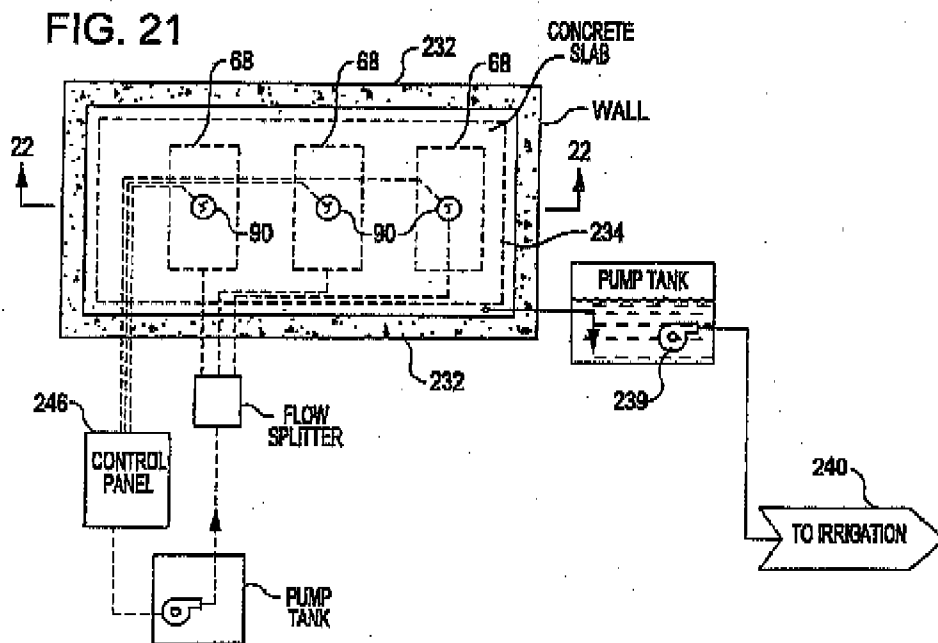
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1

COMPACT SURFACE MOUNTED ON-SITE WASTEWATER TREATMENT UNIT

RELATED PATENT APPLICATIONS

This patent application claims priority from prior U.S. Provisional Patent Application Ser. No. 60/553,819 filed on Mar. 16, 2004, entitled Compact Surface Mounted On-Site Wastewater Treatment Unit, the disclosure of which is incorporated herein in its entirety by this reference.

COPYRIGHT RIGHTS IN THE DRAWING

A portion of the disclosure of this patent document contains material that is subject to copyright protection. The applicant no objection to the facsimile reproduction by anyone of the patent document or the patent disclosure, as it appears in the Patent and Trademark Office patent file or records, but otherwise reserves all copyright rights whatsoever.

TECHNICAL FIELD

This invention relates to apparatus for the treatment of wastewaters, and in particular, to apparatus for the treatment of wastewaters such as sewage via biological processes in on-site systems.

BACKGROUND

Methods and apparatus for the treatment and purification of wastewaters such as domestic sewage using a biological filter has been taught in my previous patents, namely U.S. Pat. No. 4,997,568, issued Mar. 5, 1991 for a Process and Apparatus for a Biological Reactor to Purify Water, U.S. Pat. No. 5,281,332 issued Jan. 25, 1994 for a System for Treating Sewage or Other Fluids, and U.S. Pat. No. 5,632,896, issued May 27, 1997, for a Method for Treating Sewage and Other Liquids; the disclosures of each one of the just mentioned U.S. patents is incorporated herein in their entirety by this reference. Since the time of development of such devices, however, sewage and waste water disposal requirements have continued to become stricter. And, the need for compact, highly efficient treatment systems at remote or difficult sites has grown, especially as second homes are built at remote locations or difficult site specific issues, such as steep slopes or poor draining soils. Thus, the provision of systems for small scale, on-site sewage treatment has become increasingly important at remote locations which are not served by sewers. This is especially true at locations which are on or adjacent to sensitive areas, or which are located where the native soils are not conducive to installation of traditional drain fields for sewage treatment. Also, in order for traditional on-site septic systems to work well, certain minimum soil and ground water conditions are necessary, and rather large lot sizes are often required. Locations meeting such requirements are becoming less and less available, and even when they are available, they are more and more expensive. Thus, there has been an increasing demand for high performance on-site sewage treatment systems, including for designs such as those which are taught in my prior art patents that were just noted above.

However, during the course of installation and maintenance of my prior art sewage treatment systems, I have noted an increasing and as yet still unmet need for a still more compact high performance on-site sewage treatment system. I have also noted a need for a system which

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eliminates the need to dig a hole into the native soil in order to install the apparatus. And, in some situations, it would be advantageous for an on-site wastewater treatment unit to be suitable for relocation to another spot on the same property, or to another piece of land at another location. Moreover, many of the compact aerobic residential on-site sewage treatment systems sold by others have unacceptably low performance, even when relatively new, as shown by various studies such as described by the article entitled "Aerobic Residential Onsite Sewage Systems: An Evaluation of Treated-Effluent Quality," by M. Maxfield, et al, in Journal of Environmental Health, October 2003, pp. 14-19. In that study, in which samples from 184 residences with on-site sewage treatment systems were tested (and in which seventy seven percent (77%) of the units were less than one year old), it was shown that over a third of the three common brand name units installed, namely Multi-Flu™, NorweCo™, and Whitewater™ brand systems, failed to meet the National Sanitary Foundation (NSF) certification standards for biological oxygen demand (BOD₅) and total suspended solids (TSS) in the treated effluent. And, over two-thirds of the systems failed to meet the Washington State Board of Health Treatment Standard 2 for BOD₅ and TSS. Furthermore, an average of 59% of the systems failed to meet Washington State standards for fecal coliform in the treated effluent. Consequently, there still remains an as yet unmet need for a compact, high performance on-site wastewater treatment apparatus which produces nearly undetectable levels of the common sewage contamination parameters including odor, fecal coliform bacteria, biological oxygen demand, and total suspended solids, and which produces a purified water product that can be disposed of without concern for human contact or environmental pollution.

BRIEF DESCRIPTION OF THE DRAWING

In order to enable the reader to attain a more complete appreciation of the invention, and of the novel features and the advantages thereof, attention is directed to the following detailed description when considered in connection with the accompanying figures of the drawing, wherein:

FIG. 1 provides a vertical cross-section view of a prior art on-site wastewater treatment system which generally employs the principles taught by my prior art patents listed above.

FIG. 2 provides a vertical cross-section view of my new wastewater treatment system, showing modifications and improvements to the septic tank and the pump tank, and also now including a novel surface mounted final wastewater treatment module which incorporates a surface mounted basin, a standpipe for receiving wastewater to be treated, a distribution pipe situated in the basin and connected to the standpipe for receiving and distributing wastewater to be treated, a packing in the basin for allowing biological treatment, a first or coarse screen above the packing in the basin, a second or fine screen above the coarse screen, which coarse screen is suitable for retaining thereabove a coarse sand layer located within the basin, and a medium sand layer in the basin above the coarse sand layer, and additional medium sand extending vertically and laterally beyond the basin so as to provide a sloping outer sidewall along the sides and along the ends of the basin, and where the sloping sidewall extends downward toward and in most suitable situations to the native soil, so that an absorption footprint is provided for transport of the treated wastewater to the native soil.

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FIG. 3 provides a partial exploded perspective view of some of the elements included in my final surface mounted wastewater treatment module, including a watertight basin having an upper overflow rim, and in this case, wherein the basin is mounted on scarified native soil, and a standpipe for receiving wastewater to be treated, a distribution pipe situated in the basin and connected to the standpipe for receiving and distributing wastewater to be treated, a packing in the basin for allowing biological wastewater treatment, an upper coarse screen above packing in the basin, a fine screen above the upper coarse screen, the fine screen suitable for retaining thereabove a coarse sand layer, then a coarse sand layer above the fine screen and within the basin, and then a medium sand layer in the basin above the coarse sand layer, and additional medium sand extending vertically and laterally beyond the basin so as to provide a sloping outer sidewall along the sides and along the ends of the basin, and where the sloping sidewall extends downward toward and in most suitable situations to the native soil, so that an absorption footprint is provided for transport of the treated wastewater to the native soil.

FIG. 4 is an enlarged vertical cross-sectional view, similar to that first shown in FIG. 2, but now showing in detail the path of wastewater through the compact surface mounted final wastewater treatment module, from the inlet transport line, to the standpipe for receiving wastewater to be treated, to the distribution pipe situated in the basin and connected to the standpipe for receiving and distributing wastewater to be treated, to the packing in the basin for allowing biological treatment, through the first or coarse screen above the packing in the basin, then upward through the second or fine screen above the coarse screen, then upward through a first media layer which in one embodiment is provided by way of a coarse sand, and then upward within the basin through a second media layer which in one embodiment is provided by way of a medium sand, then upward and outward over the rim of the basin and thence through at least one media layer to an outer layer, which in one embodiment can be provided by further addition of a medium sand to and above the second media layer, and then further outwardly and downwardly through the at least one outer media layer, and thence through an absorption foot and into the native soil below.

FIGS. 5 and 6 show how the final treatment module is situated in essentially level ground, i.e., locations in which the ground slopes from about 0 to about 5%, wherein the entire area below the outer media layer and external to the basin is available as an absorption foot.

First, FIG. 5 provides a plan view footprint of the basin as mounted on-site at the surface above a scarified native soil, and illustrates use of a suitable sand to provide an absorption footprint extending outwardly from the basin along an absorption length and an absorption width, to provide a selected absorption area, which absorption area is equal to the absorption width times the absorption length, less the basin width times the basin length.

Next, FIG. 6 provides a vertical cross-section view of the basin just illustrated in FIG. 5, when the final wastewater treatment unit is surface mounted on native soil, showing the use of a suitable sand on native soil to provide an absorption width below the basin and mound.

FIGS. 7 and 8 show how the final wastewater treatment module is situated in sloping ground, i.e., locations in which the ground slopes from about 5% to about 20%.

FIG. 7 provides a plan view footprint of the final wastewater treatment unit including a basin as mounted on native soil in sloping ground, and illustrates use of a suitable sand to provide an absorption footprint extending outwardly, both

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downhill from the basin along an absorption length and for an additional five feet in the uphill direction, and along an absorption width, to provide a selected absorption area.

Next, FIG. 8 provides a vertical cross-section view of the final wastewater treatment unit and basin as just shown in FIG. 7, with the basin surface mounted in a sloping location in native soil, showing how the basin is lodged on the slope, and also showing the use of a suitable sand on native soil to provide an absorption area.

FIG. 9 is a perspective view of one embodiment of a suitable packing for the final treatment module, which in one embodiment can be provided in one-half inch long sections of thin wall plastic pipe such as polyvinyl chloride (PVC) or the like.

FIG. 10 is a side view of the packing just illustrated in FIG. 9.

FIG. 11 is a perspective view of one embodiment of the final wastewater treatment module for a compact surface mounted wastewater treatment system during construction, when utilizing an impervious liner below the basin and an external collection pipe, such as may be used for collection of the treated effluent for reuse.

FIG. 12 is a perspective view of one embodiment of a final wastewater treatment module during system construction, showing the basin after having been filled to the extent described for one embodiment herein with a suitable packing such as that of the type shown in FIG. 9, for biological treatment of the wastewater.

FIG. 13 is a perspective view similar to that just shown in FIG. 12 above, but now showing the addition of a first screen layer, such as may be provided by a "window screen" size of screening synthetic fabric.

FIG. 14 is a perspective view similar to that just shown in FIGS. 12 and 13, but now showing the addition of a second screen layer, such as may be provided by a "bridal veil" size of screening synthetic fabric, which second screen layer is sufficiently small in size so as to substantially prevent the migration of the first media layer, such as a coarse sand, downward through the second screen layer.

FIG. 15 is a perspective view similar to those shown in FIGS. 12, 13, and 14, now showing the addition of the first media layer of coarse sand which has in this embodiment been added above the second screen layer.

FIG. 16 is a perspective view of a finished surface mounted on-site final wastewater treatment module, showing how the final media layer is provided upward and outward from the basin to provide for transport of treated effluent upward from the basin and thence downward and outward toward either a collection system as first illustrated in FIG. 11 above, or to an absorption foot in contact with native earth, as illustrated in FIG. 4 above.

FIGS. 17, 18, and 19 illustrate various embodiments which may be utilized for enhancing the quality of the final treated effluent, especially with respect to reduction of nitrates in the treated effluent.

In FIG. 17, the use of an air bubbling system in the second compartment of a two compartment septic tank is illustrated, wherein a packed bed is provided for upward contact between air bubbles and the effluent being treated.

In FIG. 18, the use of an extended aeration media surface such as a rectangular outdoor rug is shown, wherein the extended aeration media surface is affixed to one or more walls of the pump tank, and wherein a portion of the effluent to be treated is sprayed toward the extended aeration media surface and is then allowed to trickle toward the bottom of the tank.

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In FIG. 19, instead of using an extended aeration media surface as just illustrated in FIG. 18, the effluent to be treated is sprayed against one or more sidewalls of the pump tank, and is then allowed to trickle toward the bottom of the pump tank.

In FIG. 20, the construction details of the packed column treatment device first shown in FIG. 17 above are described, now showing in this embodiment a centrally located air supply tube, which delivers air to an air delivery sparge, and a column housing as may be provided in PVC or other suitable materials.

FIG. 21 shows the use of three on-site surface mounted final wastewater treatment units operating in parallel, with the units placed on an impervious concrete slab with internal collection trenches, so that the treated effluent can be collected for reuse, for example, for irrigation service.

In FIG. 22, a vertical cross section of the three on-site surface mounted final wastewater treatment units just illustrated in FIG. 21 is provided, taken as if looking at section 22-22 of FIG. 21.

FIG. 23 shows in further detail the use of a high level alarm such as a float in the standpipes just illustrated in FIG. 21.

The foregoing figures, being merely exemplary, contain various elements that may be present or omitted from actual implementations and process configurations of the wastewater treatment apparatus and process system taught herein, depending upon the circumstances. An attempt has been made to draw the figures in a way that illustrates at least those elements that are significant for an understanding of the various embodiments and aspects of the invention. However, various other elements of unique wastewater treatment apparatus are also shown and briefly described to enable the reader to understand how various features, including optional or alternate features, may be utilized in order to provide an highly efficient, high effluent water quality in a compact, on-site, surface mounted wastewater treatment system that can be provided in a desired size and configuration for providing a long lasting and efficiently performing on-site wastewater treatment units.

DETAILED DESCRIPTION

An improved apparatus and method for treatment of wastewater, and especially for the on-site treatment of residential, is described and claimed herein. More specifically, the improvement described herein is to a treatment system which uses (1) an septic tank having two compartments, (2) an intermediate pump tank, and (3) a final biological wastewater treatment module which has a very small physical volume per gallon per day of influent wastewater to be treated, while nevertheless providing high quality treated effluent. Referring to FIG. 1, where one prior art system is depicted using the principles disclosed in my prior art patents identified above, a raw wastewater or sewage effluent is discharged (reference arrow 20) into septic tank 22 from indoor fixtures 24 via discharge conduit 26. A conventional cleanout system 28 is normally provided. To enhance performance, septic tank 22 may be provided as a two compartment septic tank having first 30 and second 32 compartments, so that flow (reference arrow 34) exits first compartment 30 and enters (reference arrow 36) the second compartment for treatment. Effluent (reference arrow 38) from the second compartment 32 transits through an outlet screen 40 and passages through septic tank outline line 42 and into pump tank 44. A pump 46 discharges wastewater via transport line 48 to a basin 50. As depicted in this FIG.

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1, prior art treatment units included a basin 50 that was recessed a distance D into the ground 52, with the distance D often running in the range of about two feet to about four feet, more or less, depending upon the dimensions of the basin and the treatment system capacity, as well as the soil type. In that prior art design, the rim 54 of the basin 50 must be placed a suitable and variable preselected distance above the receiving surface 56 of the native earth 58. In such prior art systems, the basin 50 has typically been provided with a cement basin having an impervious liner that prevented leakage of incompletely treated wastewater to the ground 52 below the basin 50. Basins 50 are heavy, not economically transportable or moveable for long distances, and thus, are not suitable for being sold as a package unit for long distance delivery to remote sites.

Turning now to FIG. 2, a novel, compact ground surface 60 mounted final wastewater treatment module 62 has been provided. In addition, improvements have been made in the pretreatment system 63, including the revised septic tank 22' and the revised pump tank 44'. Such a final wastewater treatment module has been mounted on scarified surface 64 of native earth 66. A substantially water impermeable basin 68, which may be provided in concrete similar to basin 50 discussed above, but which in another embodiment may be manufactured of lightweight fiberglass reinforced plastic (FRP) or other suitable plastic or lightweight formable or moldable substance, is provided. As better seen in FIGS. 3 and 4, basin 68 includes a bottom 70 having a lower outer surface 70_L and an upper inner surface 70_U, upwardly extending sidewalls 72, and an upper peripheral rim 74, over which wastewater flows outwardly from the basin in the direction of reference arrows 76 (see FIG. 2). As noted in FIG. 4, the basin 68 has a rim 74 height H_R which may vary above the scarified surface 64 of the native soil 66. In many applications, a low profile height of about 30 inches will be adequate, but of course, the size and height H_R may vary depending upon soil type (i.e. whether the soil is type 1, 2, 3, 4, 5, or 6) in that different soils absorb water at varying rates, so the geometry may be altered accordingly. A plurality of units of at least one mass transfer packing media 80 is provided. Typically, a length L_M (see FIGS. 9 and 10) of one-half inch long sections of one-half inch diameter thin wall PVC (polyvinylchloride) pipe is adequate for such media, but any of one of conventional media, including the raschig ring shape as just noted or one of the variations of similar packing that is suitable for supporting growth of biota and as is known to those of ordinary skill in the art and to which this specification is addressed, may also be utilized to perform the necessary function of providing a surface for growth of biological organisms to prove the wastewater transiting through such media. The packing media 80 provides sites for biological growth without plugging of media 80, so that at least a portion of the organic matter in the wastewater may be consumed by said biological growth. Thus, the medium is provided as packing within the lower portion of basin 68 for a depth H₁, as noted in FIG. 4. The selected packing 80 is sized and shaped to comprise a surface area adapted to support the growth of biological organisms thereon, and resulting, when packed together, in a void space within the mass transfer packing 80. This is quite important, as primarily due to the packing 80, I have found such a size and shape advantageous, since the void area is considerably larger than is the case with large gravel packed beds previously utilized in prior art devices. Preferably, the solid volume occupied by the packing 80 itself is less than about 33% of the total volume of space filled by the packing 80, and

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by the packing itself is less than about a 15% of the volume occupied by the packing itself, and yet more preferably, the solid volume occupied by the packing itself is less than about 5% of the space filled by the packing 80 itself, or even more preferably less than about 4% of the space filled by the packing 80 itself. This void space percentage is a key measure which allows compact unit operation and which is uniquely provided in the present invention. By way of comparison, the prior art system shown in FIG. 1 and discussed above and having a gravel fill in the basin 50 has a basin 50 volume of about 2.2 cubic feet per gallons of influent per day to be treated, whereas in the present invention, the basin 68 has a volume of about 1.0 cubic feet per gallon of influent per day to be treated. Yet, the residence time of influent liquid in the prior art system and in the present invention are comparable, with such residence time being about 1 hour per gallon per day of treatment capacity; the improved treatment module 62 utilizes a residence time of about 120 hours for a capacity of 120 gallons of influent to be treated per day, whereas the prior art configuration illustrated in FIG. 1 utilizes a residence time of about 134 hours for an equivalent 120 gallons of influent per day capacity. In each of the prior art and the improved treatment module 62 designs, the peripheral rim 74 of basins 50 or 68 will allow the treatment modules to provide acceptable treatment of influent wastewater when a rim 74 length of about 1 foot or more is provided for each four gallons per day of influent capacity.

Next, a standpipe 90 usually but not necessarily oriented substantially vertically is provided, and a distributor pipe 92 is provided at the lower end 91 of standpipe 90 and in fluid communication with the standpipe 90, are provided. The standpipe 90 is mounted to downwardly direct wastewater to be treated toward the distributor pipe 92. The distributor pipe 92 is mounted at or just above the upper bottom surface 70_U of the basin 68. The distributor pipe 92 includes a plurality of discharge outlets 94 adapted to discharge wastewater therefrom (see reference arrows 96 in FIG. 2) so that the wastewater 96 reaches the mass transfer packing media 80. For many applications, a four inch size PVC standpipe 90 and a four inch size PVC distributor pipe 92 are sufficient, especially for stand alone single house on-site sewage treatment systems.

Mounted above packing 80 and at least substantially covering an area interior to the peripheral rim 74 of the basin 68, at least one screen layer 100 is provided (see FIGS. 3, 13, and 14). The at least one screen layer 100 has, as a minimum the ability to substantially prevent a granular media such as coarse sand 102 of preselected size from downwardly penetrating the at least one screen 100 to reach the mass transfer packing 80, so as to protect the mass transfer packing media 80 against receipt of granular media thereon. In one embodiment, as illustrated in FIG. 3, the at least one screen 100 includes a coarse screen 104 and a fine screen 106. The application of a coarse screen 104 above packing 80 is shown in FIG. 13. As shown in FIG. 14, I have found it advantageous to utilize, as fine screen 106, a "bridal veil" synthetic fabric material, which material is placed over the coarse screen 104 as shown in FIG. 14. Each of the at least one screens 100, or 104 and 106 as may be provided, may include a suitably located central aperture defined by an interior edge line 108 or 108A, respectively, for passage therethrough of standpipe 90, whose outer circumference should be of comparable dimensions to the size of edge line 108 or 108A.

I have also found it advantageous for the compact ground surface mounted upflow aerobic treatment unit 62 as

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described herein to also include, as shown in FIG. 14, above the at least one screen layer 100, a first granular media 110 of preselected size, which as shown for the embodiment illustrated in FIG. 23 can be coarse sand. Then, as also shown in the embodiment depicted in FIG. 3, a second granular media 112 of a second preselected size is provided; this can be a medium sand, as shown, or alternately might be a fine sand. In any event, there is a first layer of media, usually granular such as sand, and a final layer of media, usually granular such as sand of a selected size. The final, or as depicted in FIG. 3, the second granular media 112 extends upward to a top surface portion 114. The preselected size of each succeeding granular media is a number N (where N is a positive integer) of media layers is, for the embodiments illustrated, smaller than the preselected size of the previous or N-1 media layer. As mentioned above, normally, the first granular media 110 can be made up of coarse sand. In such cases, the second granular media 112 can be provided as medium sand.

Note in FIG. 2 and in FIG. 4 that the standpipe 90 has an upper end 120, and the standpipe 90 extends vertically for a distance sufficient that the upper end 120 extends above the top surface 114 of the final granular media, which is a second media layer of medium sand 112 as depicted in FIGS. 2 and 4. As shown in FIGS. 2 and 4, the final granular media, here, second media 112, extends laterally outwardly from said basin to a peripheral edge portion 122. As shown in FIG. 4, the peripheral edge 122 adjoins scarified surface 64 of the native earth 66. As seen in FIGS. 5, and 6, for systems 62 mounted on flat ground, the peripheral edge 122 defines, inwardly of the peripheral edge, an absorption area or "foot" portion that provides a pathway for treated wastewater to enter the native soil 66 therebelow. In contrast to the prior art system shown in FIG. 1 above, in the present invention, the entire gross absorption area, that is the absorption area A_g , times the absorption width A_p , is available for infiltration of treated liquid, and no deduction in allowable area need be made for the area occupied on the soil surface by the basin of length B_L and width B_p . Thus, while in prior art, the basin 50 was recessed into the earth, the ability to locate the present system on the surface 64 of earth 66 means that gross absorption area can be utilized, rather than net absorption area, for purposes of determining availability of infiltration soil. Also, as seen in FIGS. 7 and 8, when mounted on a sloping location, in prior art, the absorption foot was only be considered to include the area downhill of the centerline 130 of basin 50, whereas with the present invention, an area having a width A_U on the uphill side of basin 68 can additionally be utilized for calculating absorption area.

I believe it to be advantageous, for packaging and transport of the treatment unit 62, before installation, to manufacture the basin 68 in a lightweight, moldable material. In one embodiment, basin 68 can be manufactured in a moldable plastic. In another embodiment, a fiberglass reinforced plastic may be utilized.

Overall, the compact ground surface mounted biological treatment unit 62 described herein is configured for upflow movement of wastewater, such that the wastewater fed to the treatment module 62 ascends from the basin 68 through said first mass transfer media 80, and thence over the peripheral rim 74 of the basin 68, and then into either a second or other selected one of N layers of media such as second granular media 112.

In the case of influent having levels of nitrates which may need additional treatment to attain a desired effluent treatment standard, there are a number of methods providing such treatment in addition to the process and apparatus

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already described. Thus, the wastewater treatment system as already described may further include a nitrate treatment step or unit.

As illustrated in FIG. 2, the nitrate treatment unit includes a recycle line 150 from the pump tank 44' to the two compartment septic tank 22'. The two compartment septic tank 22' has a riser 152 with a lid 154 above the first compartment 30 in the septic tank 22'. A water permeable container such as sack 160 having therein a plurality of packing media such as media 80 is provided within the sack 160 in the riser 152. A recycle line 160 provides recycled wastewater from the pump tank 22', and the wastewater is discharged on to the packing media 80 wherein nitrate concentration in treated effluent from said system is reduced such as by way of exposure to air and oxidation directly or indirectly. As noted above, in one embodiment, packing 80 may be provided by way of 1/2 inch lengths of 1/2 inch diameter PVC pipe.

The system shown in FIG. 17 provides nitrate treatment unit by way of an air sparged submerged packed column 170 in the second compartment 32 of the two compartment septic tank 22'. As better seen in FIG. 20, the air sparged packed column 170 has, in one embodiment, an outer cylindrical PVC shell 172, a lower retaining screen 174, an air line 176 running from an air pump 178 to a discharge opening 180 located adjacent the lower retaining screen 174, and a plurality of packing media such as media 80 the retaining screen 174 and contained within the PVC shell 172. As illustrated for this embodiment, the packing media 80 is made up of a plurality of packing pieces of 1/2 inch lengths of 1/2 inch diameter PVC pipe.

Also, as shown in FIGS. 17 and 18, in one embodiment, a suitable nitrate treatment unit includes a recycle line 160 from the pump tank 44' to a spray nozzle 200 in the riser 152 in the first compartment 30 of the two compartment septic tank 22'. Liquid in line 160 may be supplied by a single pump 46 using a flow splitter 204, or with an independent second pump 46A as seen in FIGS. 18 and 19. The spray nozzle 200 is oriented so as to aerate recycled wastewater 202 discharged from the spray nozzle 200 into the first compartment 20 of the septic tank 22'.

In yet another embodiment shown in FIG. 18, the nitrate treatment unit is provided by way of an extended surface media 210 on at least one interior 212 wall of the pump tank 44'. A recycle line 214 is provided within the pump tank 44'. The recycle line 214 provides wastewater 216 from said pump tank 44' and discharges the wastewater at nozzle 218 on to the extended surface media 216 in the pump tank 44'. An orifice 220 or other suitable flow splitter may be utilized to accomplish the split flow requirement. As illustrated in this embodiment, the extended surface media 210 can be provided in the form of a decomposition resistant outdoor rug.

In those situations normally encountered, the influent to the wastewater treatment system normally includes suspended particulates. The suspended particulates are substantially physically removed from wastewater by a number N (where N is normally two or more) of preselected granular media portions.

More generally, it should be kept in mind when reviewing this specification and the meaning of the claims below that the media 80, whenever used, maybe in the form of a raschig ring or similar packing, and may be provided in short pipe sections. The material for such pipe may be selected from the group consisting of (a) polyvinylchloride, and (b) high density polyethylene. While they have been described as being furnished in shapes and sizes of approximately one-half inch long and in pipe sections are approximately one-half inch in diameter, this is just for reference with respect to performance seen in the experimental test unit

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which underwent extensive evaluation, and is not intended to limit practice of this claimed invention to this size and shape, but merely for exemplary purposes.

Turning now to FIGS. 21, 22, and 23, it can be seen in FIGS. 21 and 22 that a plurality of wastewater treatment modules 62 can be provided on a common impervious substrate, such as a concrete slab 230, where capture and collection of treated effluent is desired for further discharge or reuse, rather than ground recharge through absorption into native earth. Where collection is practiced, a curb 232 may be provided at the perimeter of slab 230, and collection trenches 234 may be utilized for easy collection of treated effluent for discharge to a pump tank 238, where the treated effluent may be pumped via pump 239 to a desired use such as landscape irrigation 240. A plurality of wastewater treatment modules 62 can be provided using a plurality of basins 68. As shown in FIG. 21, three wastewater treatment modules 68 are provided. And as further detailed in FIG. 23, each basin can include a standpipe 90 having a level sensor 242 for sensing liquid level 244, for providing a control input to control panel 246 and regulate wastewater input rates to the treatment system.

The apparatus described herein is useful in a method of treating wastewater in a compact, on-site treatment system of the type in which wastewater is processed in a septic tank and then in a treatment bed module. Importantly, the process improvement of the development described herein is characterized in that the aerobic treatment process includes providing in one embodiment a watertight basin 68, wherein the watertight basin 68 is situated on a scarified surface 64 of a native soil 66. Water is directed from the septic tank to the standpipe, and thence to the distributor pipe. The wastewater is allowed to move upward through the mass transfer packing media 80 and thence over the peripheral rim 74 of the basin 68. The wastewater is allowed to migrate into the first media portion 110, and thence to a final media portion, which, as depicted in FIG. 2, is media 112, without saturating all of the final media portion 112 with said wastewater. The treated wastewater is allowed to flow from the final media portion 112 into said native soil 66. The wastewater is effectively treated for removal of organic matter, so as to provide a treated wastewater effluent. This is especially borne out by the detailed analytical data of testing shown in TABLE 1. In TABLE 1, it is clearly shown that BOD, Fecal Coliform, TSS, and Ammonia Nitrogen are efficiently and effectively controlled by the compact treatment module 62 described herein. Thus, it can be said that the mass transfer packing medium 80 provides sites for biological growth without plugging of the medium, so that at least a portion of the organic matter in the wastewater may be consumed by said biological growth. As the test data was actual data taken from an on-site residential application, the sewage treatment value is self evident.

Importantly, when using the apparatus and method taught herein, the treated wastewater effluent can be discharged for reuse. Treated wastewater can be absorbed in an absorption foot interface between the final medium and the native earth. For example, the treated wastewater can be directed into the scarified native earth, for recharge of local groundwater. Or, the free liquid can be collected into a storage device for reuse. Alternately, the treated wastewater effluent can be reused for landscape irrigation.

Although the coarse sand, medium sand, and optional fine sand can be of various preselected sizes, those of ordinary skill in the art and to whom this disclosure is directed will be able to effectively evaluate and select the same. For example, in one case, well washed sand with effective particle size <0.80-2.00 mm and a permeability coefficient <1.5, can be utilized without clogging through a fabric separator or screen. Then, as shown in FIG. 23, the treated

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sand with an effective particle size <0.50-0.60 mm and uniformity coefficient of <1.6 can be used.

Water produced from sewage by this invention has nearly undetectable levels of the common sewage contamination parameters including odor, fecal coliform bacteria, biological oxygen demand and suspended solids. The purified product can then be disposed of without concern for human contact or environmental pollution. It can be reused for household, industrial or irrigation purposes or, discharged safely as normal surface precipitation run-off into storm sewers, ditches, streams or lakes. No separation or setback distances need be provided from wells, surface water, buildings or property lines, nor does it need particular soil or ground water conditions, as do standard systems.

Further details confirming performance of my new system can be appreciated by a review of the test data which was obtained during an extensive on-site test, as well as comparing such data to the performance achieved by prior art systems similar to those described in my earlier patents referenced above. First, in TABLE 1, a summary of Laboratory Results and a statistical analysis is provided for the treatment of an "influent" raw wastewater from a residential site in Poulsbo, Wash. by my new "MODEL M32" wastewater treatment system as described and claimed herein. TABLE 1 also shows the "effluent" treated wastewater discharged from the system. Treatment results for BOD₅, TSS, and fecal coliform (CFU) are provided. Second, in TABLE 2, further details of data are provided from testing of my "MODEL M32" as described and claimed herein. Finally, in TABLE 3, performance data is provided from earlier testing of prior art system "MODEL M31" of the type as described in the prior art system depicted in FIG. 1. Importantly, comparable treatment performance is now available in a treatment system which does not require excavation for placement of a basin or similar treatment container; rather, as depicted especially in FIGS. 2 and 4 herein, my new "MODEL M32" system allows placement of the treatment system mound "on grade". This simplifies criteria for location of such systems, and also makes them easier to move in situations where location to new underlying absorption earth is desirable.

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Although various aspects and elements of the invention are herein disclosed for illustrative purposes, it is to be understood that the soil surface mounted upflow final wastewater treatment module as described herein is an important improvements in the state of the art of structures and materials for treating wastewater on small, on-site treatment systems. Although only a few exemplary aspects have been described in detail, various details are sufficiently set forth in the figures of the drawing and in the specification provided herein to enable one of ordinary skill in the art to make and use the invention(s), which need not be further described by additional writing in this detailed description. Importantly, the aspects and embodiments described and claimed herein may be modified from those shown without materially departing from the novel teachings and advantages provided as described herein, and may be embodied in other specific forms without departing from the spirit or essential characteristics thereof. It is especially pointed out that the size, and shape of the basin, and the amount of sand necessary to provide an absorption area of suitable size, will vary widely based on wastewater flow rates to the system and based on ground or soil conditions below the unit and into which the residual treated wastewater is absorbed. Therefore, the embodiments presented herein are to be considered in all respects as illustrative and not restrictive. As such, this disclosure is intended to cover the structures described herein and not only structural equivalents thereof, but also equivalent structures. Numerous modifications and variations are possible in light of the above teachings. It is therefore to be understood that within the scope of the appended claims, the invention(s) may be practiced otherwise than as specifically described herein. Thus, the scope of the invention(s) is as described herein and as set forth in the appended claims, and as indicated by the drawing and by the foregoing description, is intended to include variations from the embodiments provided which are nevertheless described by the broad interpretation and range properly afforded to the plain meaning of the language of the claims set forth below.

TABLE 1

Summary of Laboratory Results and Statistical Analyses¹, Glendon @ BioFilter Model M32, Poulsbo, WA

	BOD ₅ , mg/L		TSS, mg/L		Fecal Coliform, CFU	
	Influent	Effluent	Influent	Effluent	Influent	Effluent
# of Valid Samples/	39	47	40	48	39	48
Range of Samples	148-726	<1-24	9-74	<1-5	1.9×10^3 - 1600×10^3	<1-402
Average of Samples	423	5.8	34.1	1.6	2.94×10^3	13.4
# of 30 Day Mean Values ² /	35	43	36	44	36	44
Range of 30 Day Mean Values	270.5-562.1	1.8-21.7	20.0-55.8	1.0-2.3	9.6×10^3 - 922.4×10^3	1.0-34.5
Average of 30 Day Mean Values	431	6.9	33.6	1.5	274.1×10^3	2.9
Mean Values						
# of Effluent Mean Values >10/10/200/		13 of 43		0 of 44		0 of 44
# of 30 Day Means						
Range, Effluent		95.9-99.7		82.1-98.6		99.9-99.9
Removal Efficiency, %						
Effluent Range @ 95% Confidence		4.0-8.0		1.7-2.3		0-30.3
Effluent Interquartile Range		2-3		1-1.6		1-1
Median, Effluent		2		1		1
Interquartile Range						

NOTES:

¹Lab results preceded by a > or < are treated as the number reported for use in all calculations.²BOD₅ and TSS are arithmetic means. Fecal Coliform is geometric mean.

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Summary of Testing and Results

A Glendon® BioFilter Model M32 was tested at a residential site in Poulsbo, Wash. from Jul. 10, 2002 through

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May 8, 2003, a span of 302 calendar days that yielded 48 effluent data days. A summary of the independent third part laboratory's results and statistical analyses derived from these data is presented in Table 1.

TABLE 2

Glendon BioFilter Technologies, Inc.
Model M32, Mincer Road Site
Effluent Removal Efficiency and 95% Confidence Analysis

GST/WA DOH Report of M32 Testing
Oct. 16, 2003

Sample Date	Influent FC CFU x 1,000	Effluent FC	Removal	Influent BOD5	Effluent BOD5	Removal	Influent TSS	Effluent TSS	Removal
			Efficiency % FC			Efficiency % BOD5			Efficiency % TSS
<u>Baseline Test of Influent Prior to M32 Installation</u>									
May 10, 2002		NS		528	NS			NS	
Jul. 1, 2002			System Startup						
Jul. 10, 2002	48	11	99.9	396	<1	99.7	22	2.8	87.3
Aug. 1, 2002	<.001*	402	—	426	2	99.3	15	1.6	89.3
Aug. 5, 2002	322	146	99.9	148	2	98.6	24	<1	95.8
Aug. 8, 2002	>200	38	99.9	234	<2	99.1	28	5	82.1
Aug. 13, 2002	1.9	<2	99.9	297	2	99.3	30	1	96.7
Aug. 15, 2002	68	<1	99.9	303	<2	99.5	42	1.5	96.4
Aug. 20, 2002	25	<1	99.9	372	<2	99.5	34	1.2	96.5
Aug. 22, 2002	46	<1	99.9	333	<2	99.4	30	<1	96.7
Aug. 27, 2002	10	<1	99.9	522	<2	99.6	21	1.6	92.4
Sep. 12, 2002	80	<1	99.9	354	<2	99.4	22	1	95.5
Sep. 26, 2002	190	<1	99.9	360	<2	99.4	32	1	96.9
Oct. 10, 2002	17	<1	99.9	435	<2	99.5	32	<1	96.9
Oct. 14, 2002	NS	<1	—	NS	<2	—	NS	3	—
Oct. 18, 2002	NS	<1	—	NS	<2	—	NS	<1	—
Oct. 21, 2002	NS	<1	—	NS	<2	—	NS	<1	—
Oct. 24, 2002	8.3	<1	99.9	336	<2	99.4	35	2	94.3
<u>Renters Moved Out -Oct. 30, 2002. New Renters Occupied Nov. 20, 2002 - System Idle for ~20 Days</u>									
n	12	16		13	16		13	16	
*Mean	84683	38		354	2		28	2	
*Std	100118	104		93	0.3		7	1	
Deviation									
t @ 95% confidence	2.201	2.131		2.179	2.131		2.179	2.131	
Lower Bound	21,071	-17,406		298	1.84		23,771	1,467	
Upper Bound	148,295	93,406		410	2.16		28,229	2,553	
Nov. 26, 2002	11	<1	99.9	471	5	98.9	9	<1	88.9
Dec. 3, 2002	NS	<1	—	NS	19	—	NS	<1	—
Dec. 5, 2002	NS	<1	—	NS	Invald	—	NS	<1	—
Dec. 10, 2002	210	<1	99.9	423	16	96.2	19	1	94.7
Dec. 12, 2002	NS	<1	—	NS	14	—	NS	5	—
Dec. 17, 2002	NS	<1	—	NS	15	—	NS	1.5	—
Dec. 19, 2002	410	<1	99.9	423	9	97.9	17	1	94.1
Dec. 26, 2002	NS	<1	—	NS	8	—	NS	2	—
Jan. 2, 2003	1600	<1	99.9	330	7	97.9	33	4	87.9
Jan. 9, 2003	800	<1	99.9	327	8	97.6	37	<1	97.3
Jan. 14, 2003	1060	<1	99.9	642	<2	99.7	39	1	97.4
Jan. 17, 2003	1200	<1	99.9	480	<2	99.6	37	<1	97.3
-Jan. 20, 2003				<u>Shutdown/Situation Two Week Vacation</u>					
n	19	28		20	27		20	28	
cumulative									
*Mean	331958	22		385	5		28	2	
*Std	476008	80		105	5		9	1	
Deviation									
t @ 95% confidence	2.101	2.052		2.093	2.056		2.093	2.052	
Lower Bound	102,526	-9,02		336	3,022		24	1,612	
Upper Bound	561,389	53,02		434	6,978		32	2,338	
-Feb. 6, 2003				<u>Restroom Flow</u>					
Feb. 12, 2003	660	1	99.9	585	24	95.9	74	3	95.9
Feb. 18, 2003	450	<1	99.9	594	24	96	41	<1	97.6
Feb. 20, 2003	600	<1	99.9	573	20	96.3	47	<1	97.9
Feb. 25, 2003	660	<1	99.9	555	2	99.6	63	<1	98.5
Feb. 28, 2003	270	<1	99.9	315	8	97.5	47	<1	97.9
Mar. 3, 2003				<u>Renters Moved Out</u>					
Mar. 4, 2003	116	1	99.9	669	18	97.3	61	1	98.4
Mar. 6, 2003	400	<1	99.9	726	16	97.8	74	<1	98.6
n	26	35		27	34				
cumulative									

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TABLE 2-continued

Glendon BioFilter Technologies, Inc.
Model M32, Minder Road Site
Effluent Removal Efficiency and 95% Confidence Analysis

GBT/WA DOH Report of M32 Testing
Oct. 16, 2003

Sample Date	Influent FC CFU x 1,000	Effluent FC	Removal Efficiency % FC	Influent BOD5	Effluent BOD5	Removal Efficiency % BOD5	Influent TSS	Effluent TSS	Removal Efficiency % TSS
*Mean	363969	18		434	7		36	2	
*Std Deviation	419903	71		138	7		17	1	
t or Z @ 95% confidence	2.060	1.96		2.056	1.96		2.056	1.96	
Lower Bound	194.328	-5.523		379	4.647		29	1.669	
Upper Bound	533.610	41.523		489	9.353		43	2.331	
Mar 29, 2003									
New Renters Occupied House - System Idle for ~36 Days									
Apr. 7, 2003	360	<1	99.9	NS	<2	—	38	1	97.4
Apr. 10, 2003	360	<1	99.9	360	2	99.4	31	<1	96.8
Apr. 15, 2003	130	<1	99.9	312	<2	99.4	23	2	91.3
Apr. 17, 2003	70	<1	99.9	591	<2	99.7	34	<1	97.1
Apr. 21, 2003	60	<1	99.9	336	<2	99.4	30	4	86.7
Apr. 23, 2003	40	<1	99.9	357	<2	99.4	35	3	86.6
Apr. 24, 2003	10	<1	99.9	423	<2	99.3	30	<1	96.7
Apr. 28, 2003	40	<1	99.9	417	<2	99.3	39	1	97.4
Apr. 30, 2003	420	<1	99.9	267	<2	99.2	27	1	96.3
May 1, 2003	420	<1	99.9	492	<2	99.6	26	<1	96.2
May 5, 2003	36	<1	99.9	429	<2	99.3	22	1	95.5
May 7, 2003	28	<1	99.9	327	<2	99.4	34	1	97.1
May 8, 2003	25	<1		456	<2	99.6	28	<1	96.4
End of Testing									
n cumulative	39	48		39	47		40	48	
*Mean	293903	13		423	6		34	2	
*Std Deviation	367313	61		125	7		14	1	
Z @ 95% confidence	1.960	1.96		1.96	1.96		1.96	1.96	
Lower Bound	178.621	-4.258		384	3.999		30	1.717	
Upper Bound	409.185	30.257		462	8.001		38	2.383	

NOTES ON STATISTICAL ANALYSIS

For simplicity, all Mean Values have been rounded to the nearest integer.
For sample sizes less than 30, t is used. The t value is based on n - 1 degrees of freedom. Z is used for sample sizes equal to or greater than 30. At 95% confidence level, both t and Z contain 0.025 in each tail.
Confidence Interval = $\bar{y}_{\text{me}} \pm cr - [t \text{ or } Z] (s/n^{0.5})$, where \bar{y}_{me} is the sample mean; s is the sample standard deviation [the sum of the squared deviations divided by (n - 1)], and $n^{0.5}$ is the square root of the number of samples.
All Lower Bound values that are minus (-) are interpreted as a lower bound of zero (0).

TABLE 3

GLENDON BIOFILTER TECHNOLOGIES, Inc.
Modular BioFilter, Model M31
Statistical Analysis

GBT/WA DOH Report of M32 Testing,
Oct. 16, 2003

Date	Influent FC CFU x 1,000	Effluent FC CFU	Removal Efficiency % FC	Influent BOD ppm	Effluent BOD ppm	Removal Efficiency % BOD	Influent TSS ppm	Effluent TSS ppm	Removal Efficiency % TSS
Nov. 28, 1995		13			20			14.4	
Nov. 30, 1995		14		180	12			17.2	
Dec. 5, 1995		10			11			6.6	
Dec. 7, 1995		9			12			2.8	
Dec. 12, 1995		80			<4			29.7	
Dec. 19, 1995		20			<5			9.1	
Dec. 21, 1995	>200	36	99.982%	200	4	98.000%	60.7	3.3	94.563%
Dec. 28, 1995		6			4			2.3	
Dec. 28, 1995	360	4	100%		NR**		66.7	5.2	97.20%
Jan. 2, 1996		14			3			5	
Jan. 4, 1996	250	11	99.996%	200	<3	98.500%	39	5.2	88.667%
Jan. 9, 1996		12			<3			6.6	
Jan. 11, 1996		2			<3			6.4	
Jan. 16, 1996		8			<3			4.6	
Jan. 18, 1996	244	12	99.995%	190	<5	97.368%	75	<0.2	99.733%

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TABLE 3-continued

GLENDON BIOFILTER TECHNOLOGIES, Inc. Modular BioFilter, Model M31 Statistical Analysis										
GBT/WA DOH Report of M32 Testing, Oct. 16, 2003										
Date	Influent FC CFU × 1,000	Effluent FC CFU	Removal Efficiency % FC	Influent BOD ppm	Effluent BOD ppm	Removal Efficiency % BOD	Influent TSS ppm	Effluent TSS ppm	Removal Efficiency % TSS	
Jan. 23, 1996		12			<3			5		
Jan. 25, 1996		3			<3			2.6		
Jan. 30, 1996		4			<3			0.6		
Feb. 1, 1996		4			<3			0.2		
Feb. 6, 1996		8			<3			11.5		
Feb. 8, 1996		12			<3			7.4		
Feb. 13, 1996		1			<3			3.8		
Feb. 20, 1996	990	6	99.999%	180	<4	97.777%	34	5	85.294%	
Feb. 22, 1996		0			<4			3.4		
Feb. 27, 1996		2			<4			0.4		
Feb. 29, 1996	770	2		160	<3	98.125%	28	0.2	99.286%	
Mar. 5, 1996		2			<3			0.8		
Mar. 7, 1996	700	0	100%	310	<3	99.03%	34	0.8	97.647%	
Mar. 12, 1996		0			<3			1.4		
Mar. 14, 1996		6			2			1		
Mar. 19, 1996		0			<3			0.6		
Mar. 21, 1996		2			<3			<0.3		
Mar. 26, 1996		6			5			1.4		
Mar. 28, 1996	253	4	99.998%	NR**	NR**		57	1	98.246%	
Apr. 2, 1996		1			<3			1		
Apr. 4, 1996		0			<3			1.1		
Apr. 9, 1996		0			<3			1		
Apr. 11, 1996	680	0	100%	180	<3	98.23%	45	<0.2	95.555%	
n		38			36			38		
Mean		8.57			4.56			4.72		
Std Deviation		13.857			3.605			7.07		
Z @ 95% confidence		1.96			1.96			1.96		
Lower Bound		4.17			3.38			2.47		
Upper Bound		12.99			5.74			6.97		
Apr. 14-27, 1996				Two Week Shutdown						
Apr. 28, 1996				Resumed Influent Flow						
Apr. 30, 1996		0			<4			8		
May 2, 1996	1320	0	100%	160	<4	97.50%	69	7.2		
May 7, 1996		1			<3			1.8		
May 9, 1996		0			<4			0.8		
May 14, 1996		2			<4			1.8		
May 16, 1996		0			<4			1.8		
May 21, 1996	9200	6	100%	200	<4	98.00%	66	2		
May 23, 1996		0			<4			2		
May 25, 1996										
All Samples										
n		46			44			46		
Mean		7.82			4.43			4.26		
Std Deviation		12.91			3.27			6.5		
Z @ 95% confidence		1.96			1.96			1.96		
Lower Bound		3.55			3.46			2.38		
Upper Bound		11.01			5.40			8.14		

Notes:

Lab results preceded by a > or < are treated as the number reported for use in all calculations.

NR**--Not Reported

The invention claimed is:

1. A wastewater treatment module for treating contaminated wastewater in a biologically active treatment bed, said apparatus comprising:

(a) a substantially watertight basin, said basin having an outer bottom surface adapted for placement on a substrate, an inner bottom surface, and upwardly extending

sidewalls, and a peripheral rim having a selected elevation above said bottom, said basin having a selected containment volume V_1 ;

(b) a plurality of units of at least one mass transfer packing media located within said basin, said mass transfer packing media sized and shaped to comprise a surface area adapted to support the growth of biological organisms thereon, and a selected containment volume V_2 .

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- (e) providing, above said at least one screen layer, a granular or porous filter media having interstitial pores, said granular or porous filter media further comprising two or more preselected media portions, said two or more preselected media portions comprising at least (A) a first media portion, and (B) a final media portion, said final media portion being finer in size than said first media portion;
- (f) directing said wastewater to said septic tank;
- (g) directing said wastewater from said septic tank to said standpipe, and thence to said distributor pipe;
- (h) allowing said wastewater to move upward through said at least one mass transfer packing media;
- (i) allowing said wastewater to migrate upward into said first media portion;
- (j) allowing said wastewater to flow from said first media portion to said final media portion, without saturating all of said final media portion with said wastewater;
- (k) allowing said wastewater to flow from said final media portion to said substrate;
- (l) wherein said wastewater is effectively treated for removal of organic matter, so as to provide a treated wastewater effluent.
55. The method as set forth in claim 54, wherein said wastewater passes through a separator between said mass transfer packing and said preselected media portions, said separator substantially preventing said preselected media portions from migrating into adjacent preselected mass transfer media.
56. The method as set forth in claim 54, wherein said wastewater further comprises suspended particulates, and wherein said suspended particulates are substantially physically removed from said wastewater by said two or more preselected media portions.

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57. The method as set forth in claim 54, wherein said mass transfer packing media provides sites for biological growth without plugging of said media, so that at least a portion of said organic matter in said wastewater may be consumed by said biological growth on said mass transfer packing media.

58. The method as set forth in claim 54, further comprising the step of allowing ambient air to pass through said unsaturated final media portion to evaporate a portion of said wastewater.

59. The method as set forth in claim 54, wherein said wastewater comprises sewage effluent.

60. The method as set forth in claim 54, wherein said first media portion is comprises coarse sand.

61. The method as set forth in claim 54, wherein said final media portion comprises fine sand.

62. The method as set forth in claim 61, wherein said fine sand has an effective particle size from about 0.50 mm to about 0.60 mm.

63. The method as set forth in claim 62, wherein said fine sand has a uniformity coefficient of less than about 1.5.

64. The method as set forth in claim 54, wherein said treated wastewater effluent is collected for reuse.

65. The method as set forth in claim 64, wherein said collected treated wastewater is stored for reuse.

66. The method as set forth in claim 65, wherein said treated wastewater effluent is reused for landscape irrigation.

67. The method as set forth in claim 54, wherein said treatment module is at least partially situated on a scarified surface native earth, and wherein said treated wastewater is directed into said scarified native earth, for recharge of local groundwater.

* * * * *